Tappi PLACE Extrusion Coating and Blown/Cast Film Short Course

August 24th-26th, 2010 Charleston, SC

Fundamental Concepts of Extrusion Design

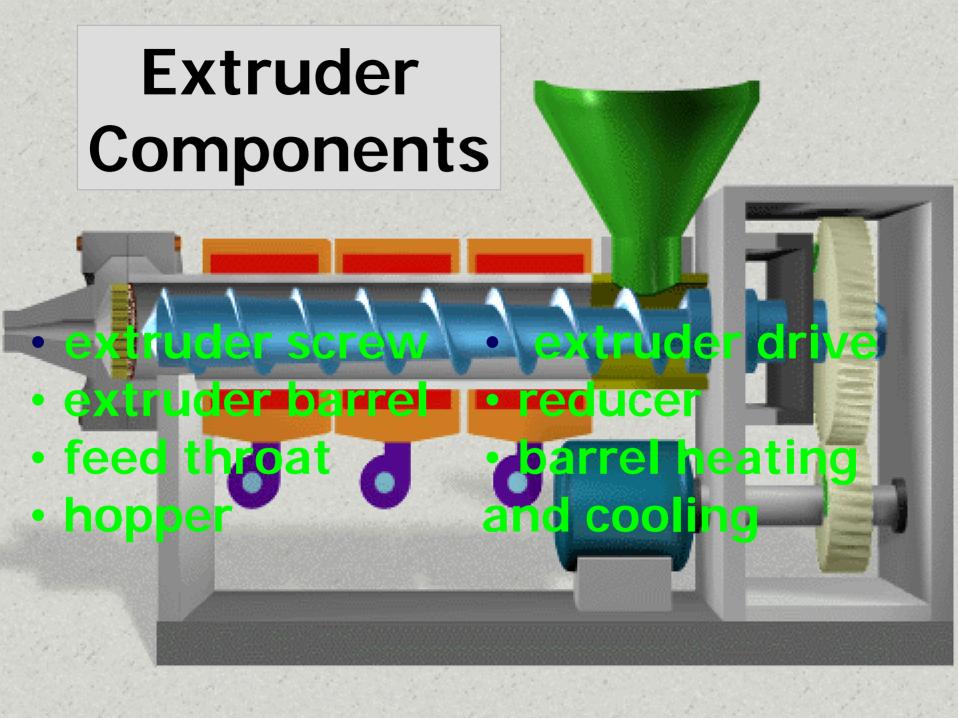
Presented By:
Lou Piffer

Davis-Standard Corp.









AC / DC Drives & Motors

Drive Motor

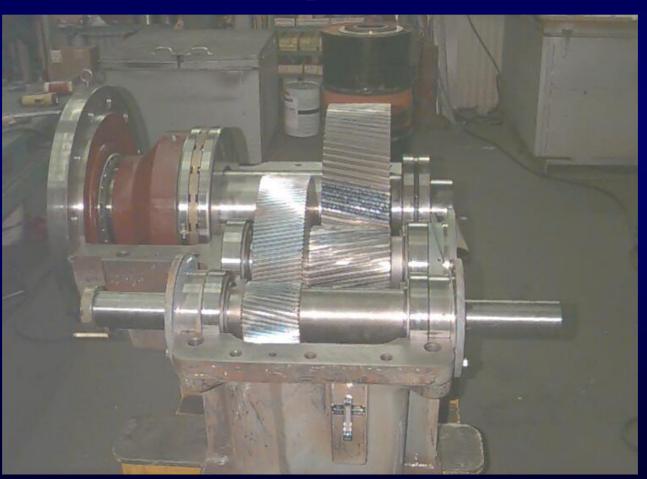
- 6" 400/500 HP
- 4 1/2" 250 HP
- 3 1/2" 150 HP
- 2 1/2" 75 HP



GearBox

Gearbox

• Converts high speed output shaft from drive (1750 RPM) to screw speed

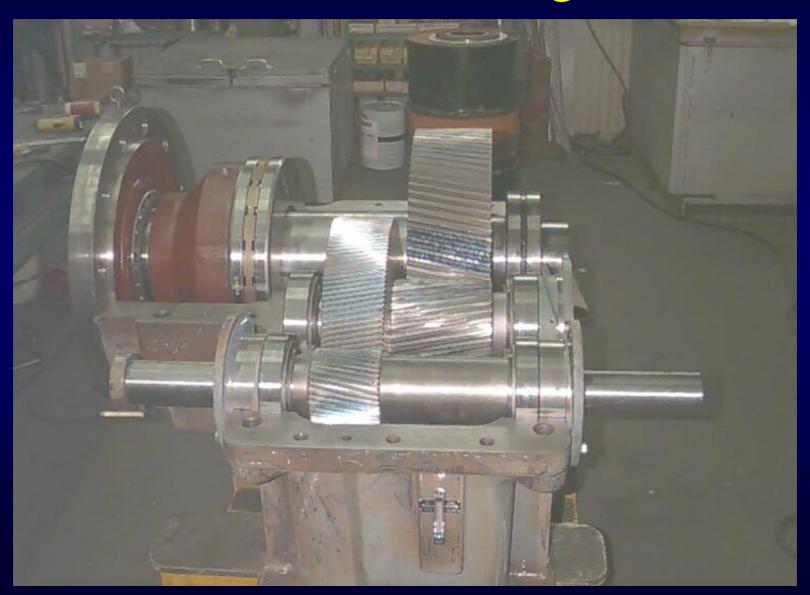


Gearbox

 Closed loop oil circulation system insures gears do not see excessive heat



Thrust bearing



B-10 Life

Expected Life of 9 out of ten bearings at a given condition

Predictive Maintenance

- Bronze in oil out of round thrust bearing
- Steel in oil bad bearing or gear tooth
- Cast iron powder in oil moving part against gear box casting

Feedsection

Feed Section

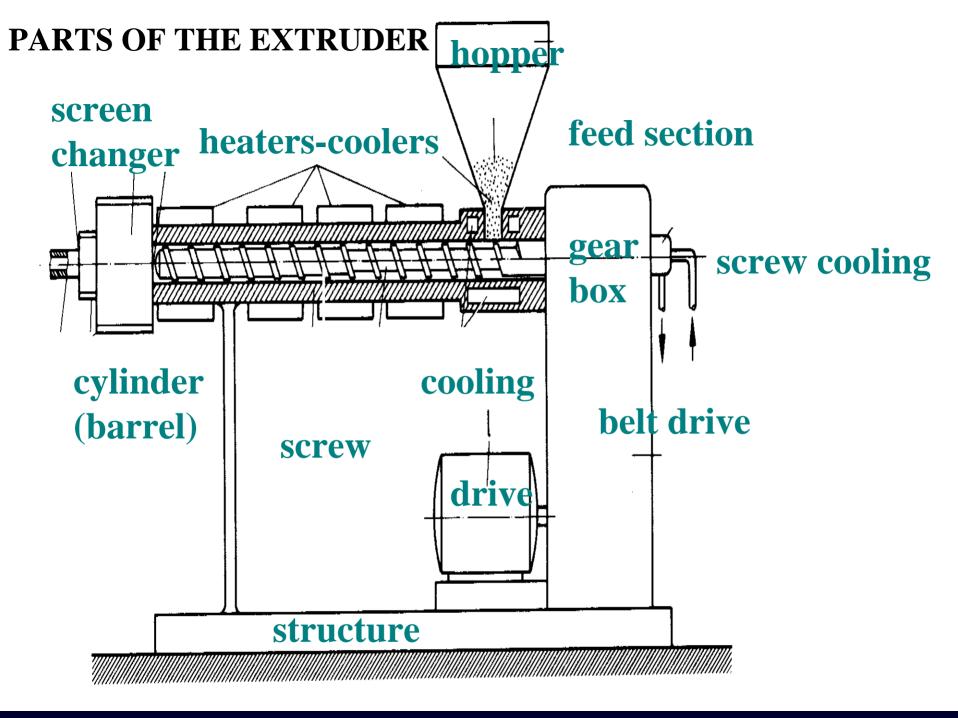
- Cast iron jacketed
- Initial point where resin is introduced
- Space between gear box and resin feeding point



Resin Hopper

Hopper often cooled to prevent bridging





Extruder Barrel

- 1/16" Bimetalic Alloy
- Bolted to feedsection
- The barrel is harder than the screw.
- Sliding barrel support



Barrel Types

- Non abrasive environments Chromium-modified boron-iron alloy.
- Abrasive environments Tungsten carbide in a matrix of nickel alloy.
- Abrasive style barrel may cost 25% more but last 3X longer!

Barrel Wear

- 1/16" (.0625") thick when new
- Should look at replacing barrel when there has be .030" of wear.

Screw Wear

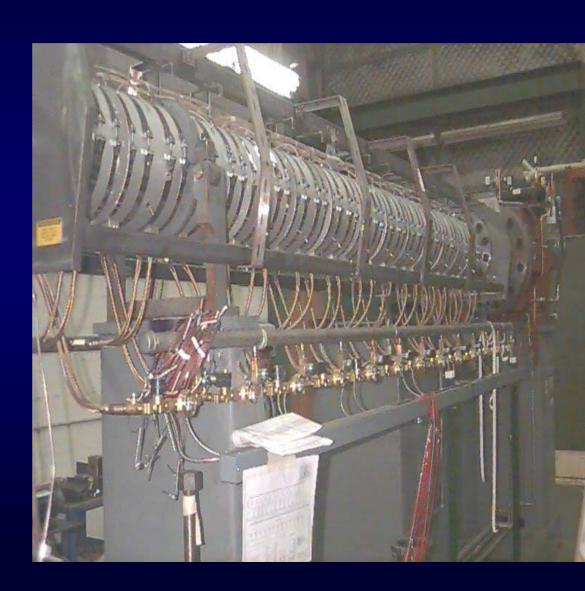
- Initial clearance of 1 mil/extruder diameter/side
- Example . 4.5" extruder will have initial clearance of approximately .0045/side
- Look to replacing screw when clearance doubles to triples. (In above example when clearance is .009 .0135")

Barrel Heater Types

- Ceramic Band (heat only)
- Electric Heat Air Cooled
- Electric Heat Water Cooled

Water cooled Heaters

- Jacketed Heater
- Solenoid valves
- Inlet/outlet manifolds.
- Water reservoir



Water cooled Heaters

- Jacketed Heater
- Solenoid valves
- Inlet/outlet manifolds.
- Water reservoir



Air cooled Heaters

- Finned Heater
- Air Blowers



Air cooled Heaters



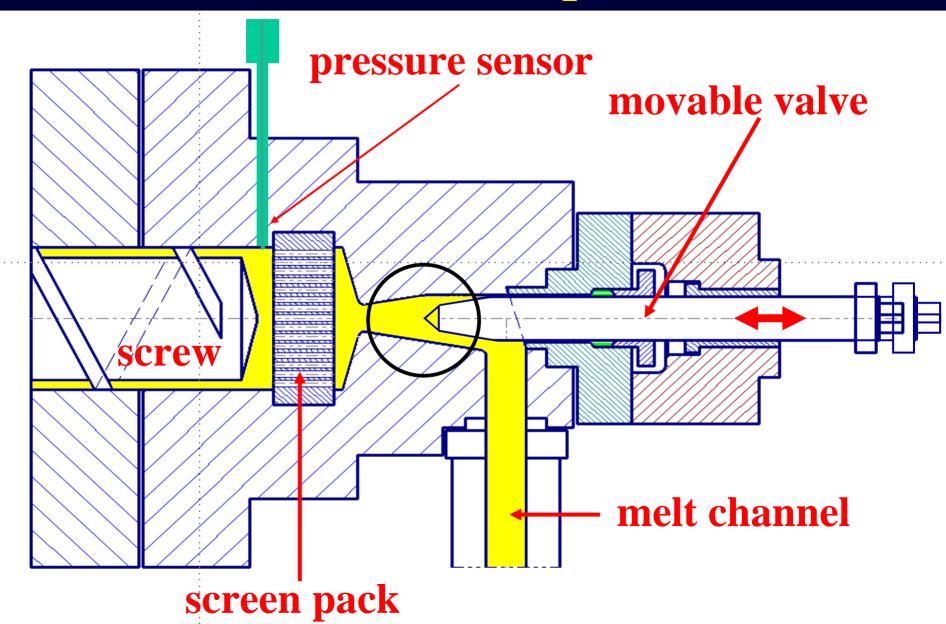
Extruder Adapter

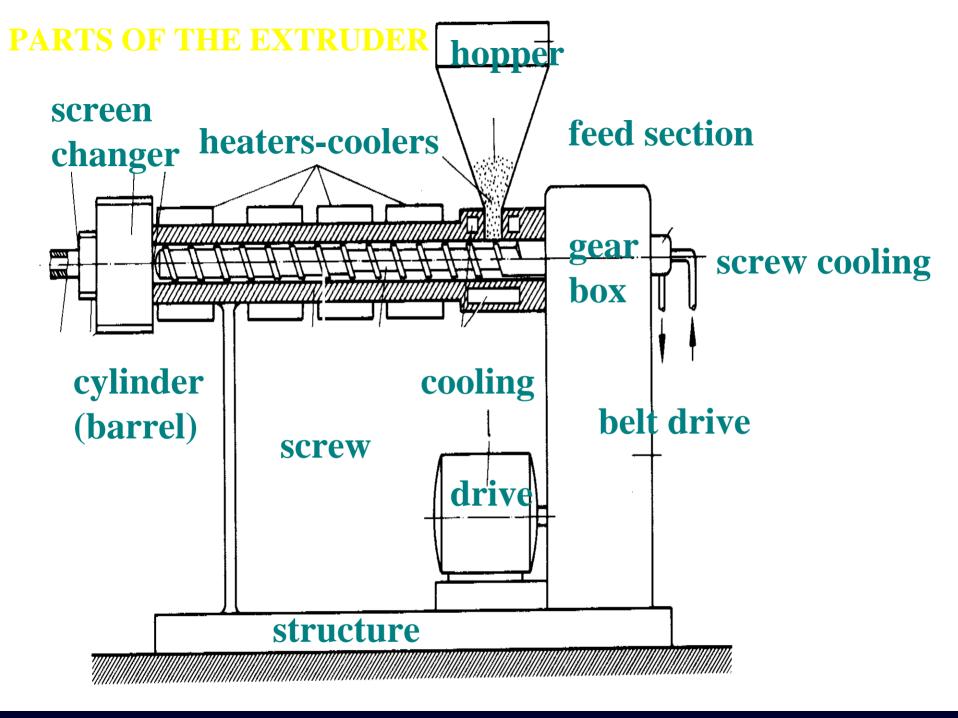
Extruder Adapter

- Change resin flow
- Change pressure
- House screen pack



Valved Adapter

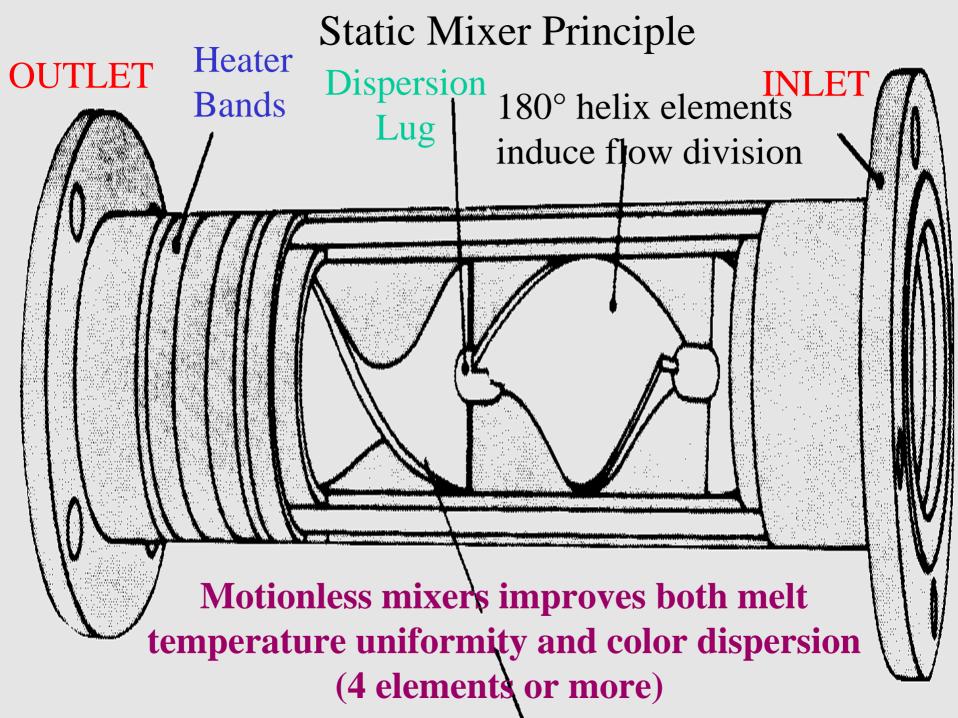




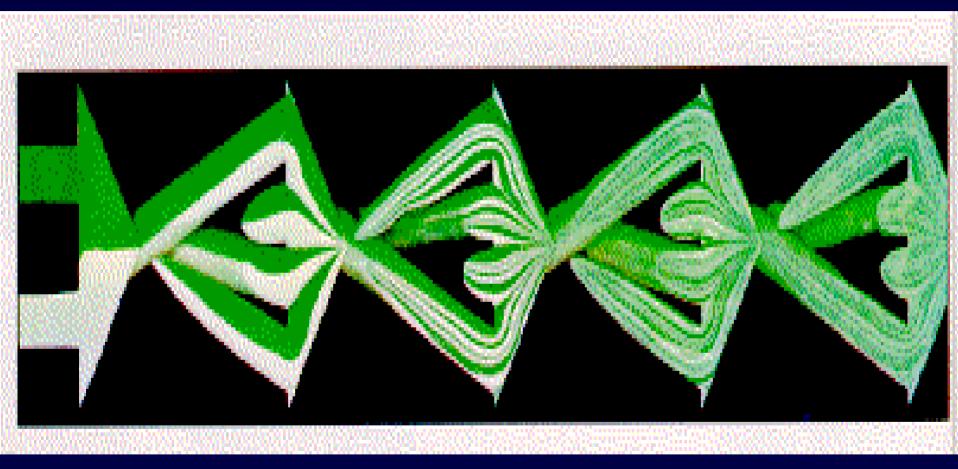
Extruder Adapter

- Change resin flow
- Change pressure
- House screen pack





Static Mixer Principle



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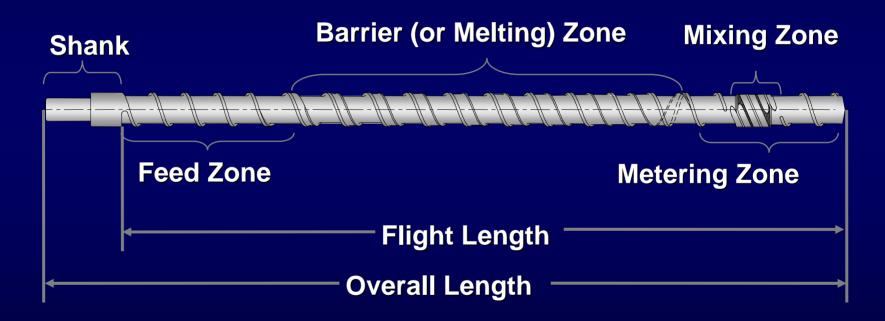
What will I learn?

- Why can't my screw run all resins?
- Why are barrel profiles unique to a screw design?
- Why can increased barrel temperature sometimes result in less output?
- What happens when my screw wears out?

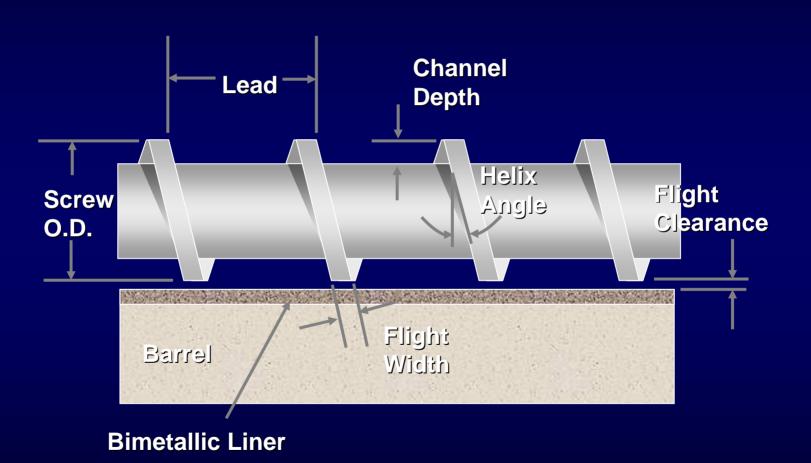
Viscous Heat Generation

Heat = Viscosity x Shear Rate²

Screw Terminology



Screw Terminology



Typical Screw Classifications

Metering Screw



Mixing Screw



• Barrier Screw



Important Ratio Terms

- L/D = Length/Diameter
- CR = Compression Ratio

CR = Feed Channel Depth

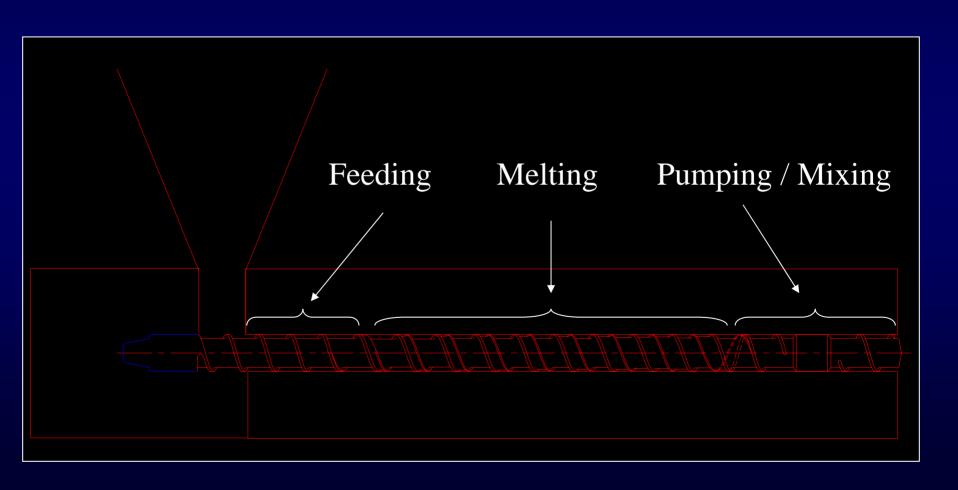
Meter Channel Depth

 Compression Ratio has no meaning for barrier type screw designs

Primary Functions of a Single Screw Extruder

- Optimized screw design must accomplish
 - Solids Conveying
 - Melting
 - Pumping
 - Mixing
- Each component is critical to the extrusion process

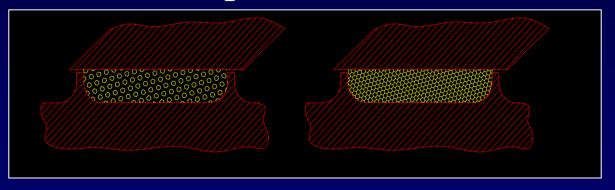
Primary Functions of a Single Screw Extruder



Feeding/Solids Conveying

Solids Conveying

• Formation of a compacted solid bed





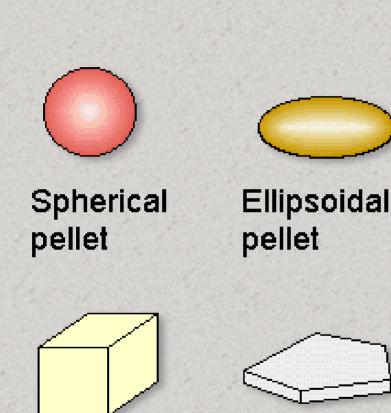
Some of the Most Important Bulk Properties:

- bulk density
- compressibility
- internal coefficient of friction
- external coefficient of friction
- particle size and particle distribution
- particle shape and particle distribution

Plastic Forms for Extrusion

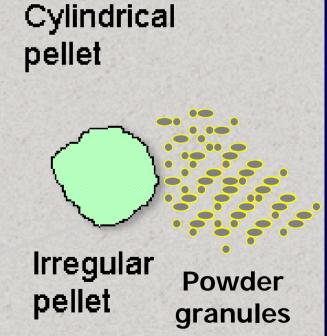
Film

scrap



Cubical

pellet



Resin Hopper

Hopper often cooled to prevent bridging



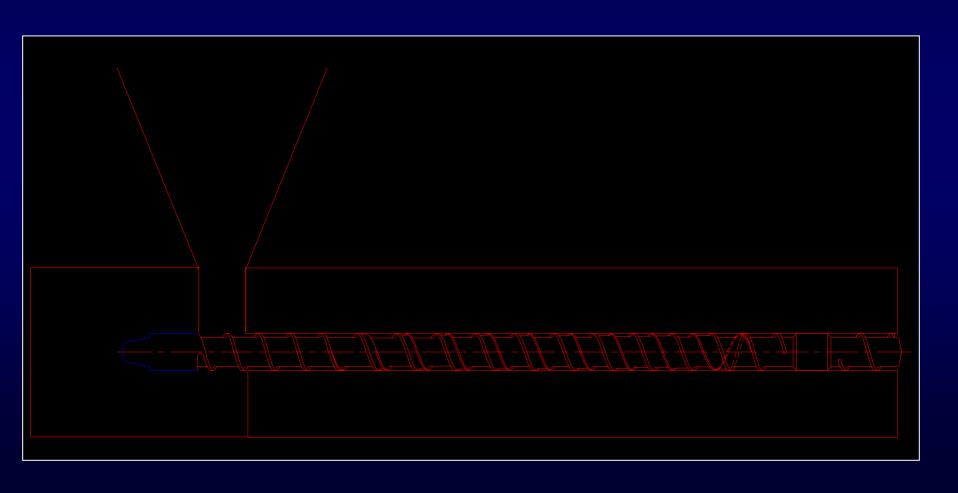
Drag Induced Conveying

The frictional force <u>at the barrel</u> is responsible for moving the material forward

For efficient forward conveying we want high friction on the barrel and low friction on the screw

If there is no barrel friction, then there can be <u>no</u> forward conveying

Solids Conveying

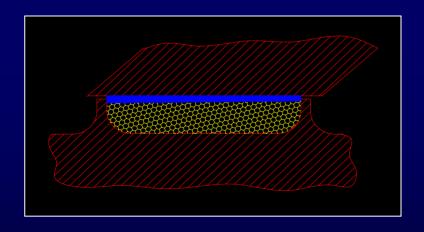


A wide distribution in particle size makes the material more difficult to convey and can lead to separation

Melting

Melting

- Formation of a compacted solid bed
- Development of a melt film







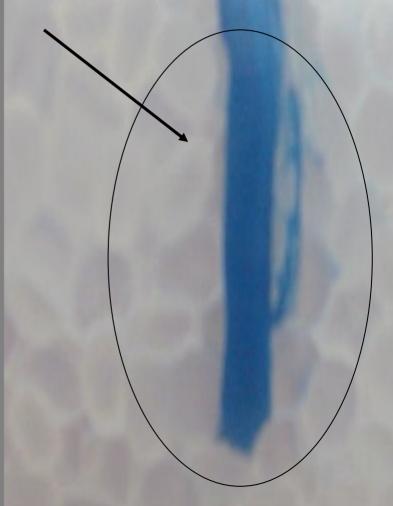
Mechanical Deformation

Melt Film / Solid Bed

Interface

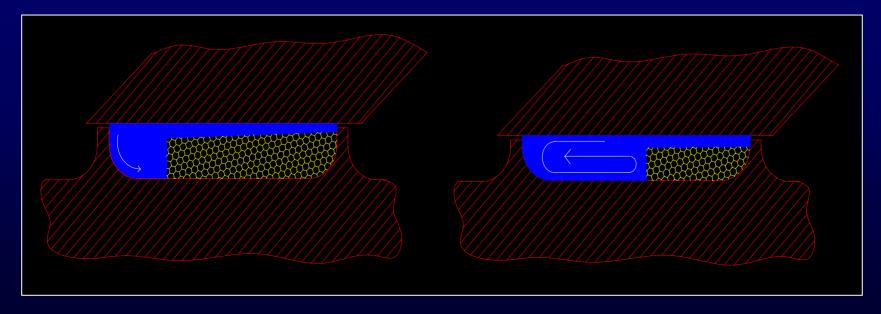
Melt Film / Barrel Wall Interface

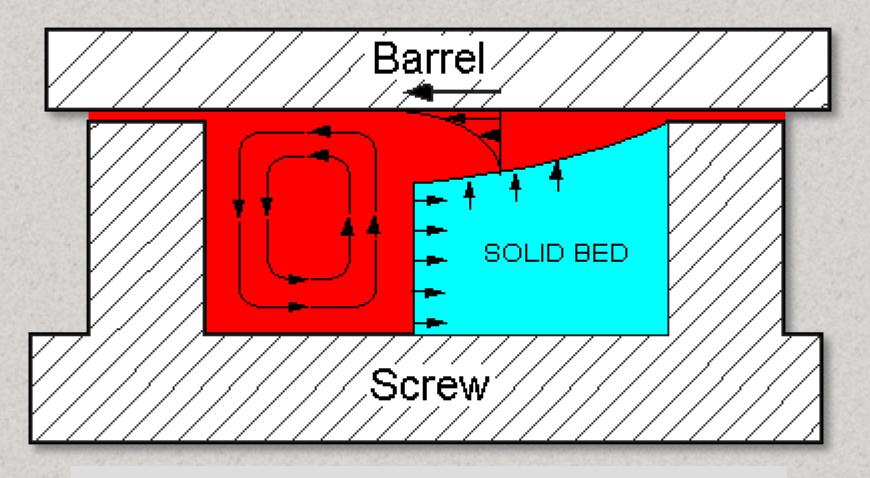
Conductive Melting w/ Forced Melt Removal



Melting

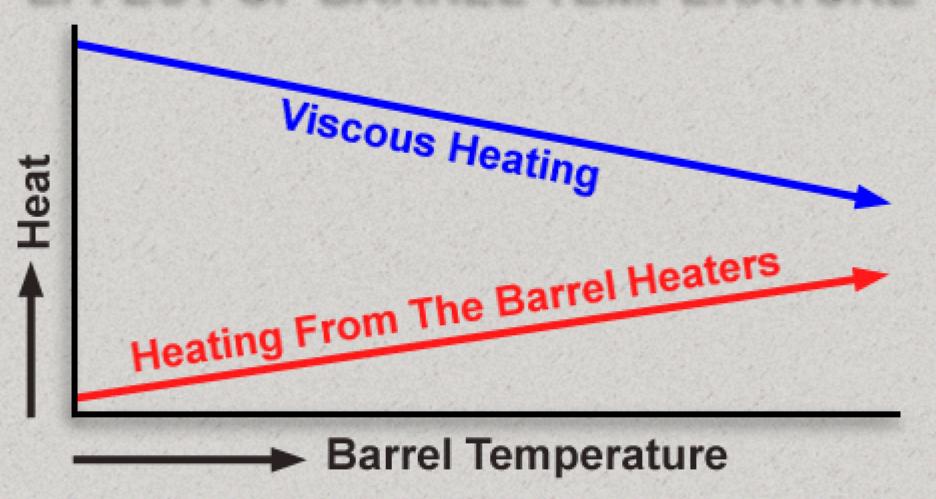
- Formation of a compacted solid bed
- Development of a melt film
- Removal of melt into an accumulating melt pool





Contiguous Solids Melting

EFFECT OF BARREL TEMPERATURE

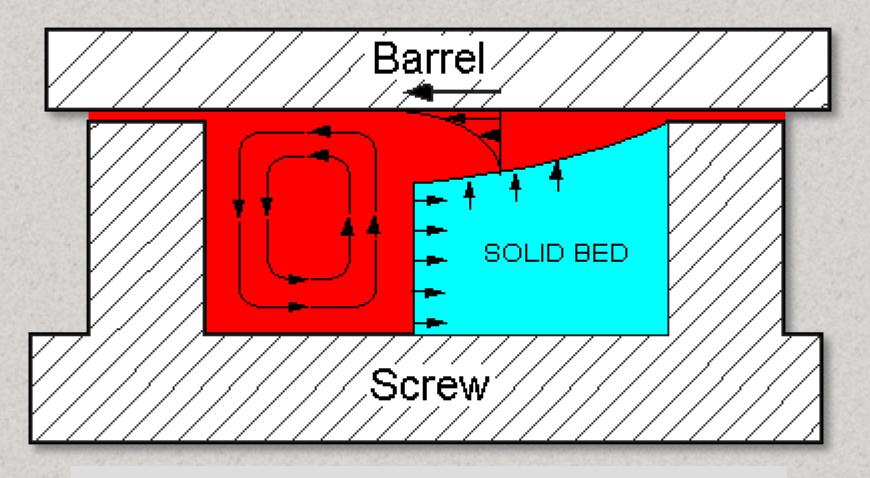


Viscous Heat Generation

Heat = Viscosity x Shear Rate²

Factors that effect the melt rate

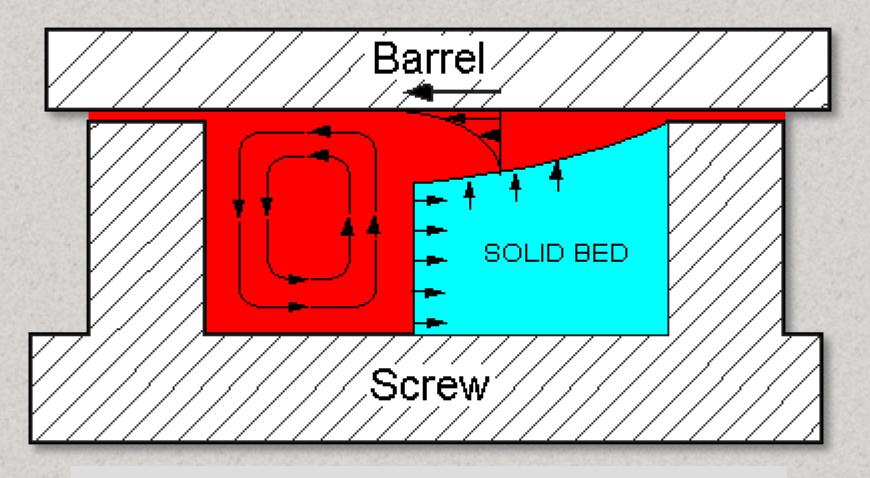
• Melt Film Thickness



Contiguous Solids Melting

Factors that effect the melt rate

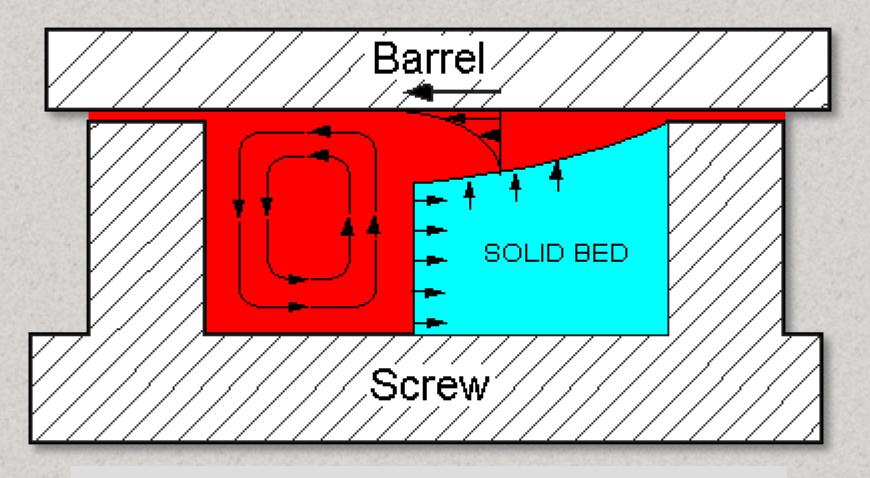
- Melt Film Thickness
- Barrel Temperatures



Contiguous Solids Melting

Factors that effect the melt rate

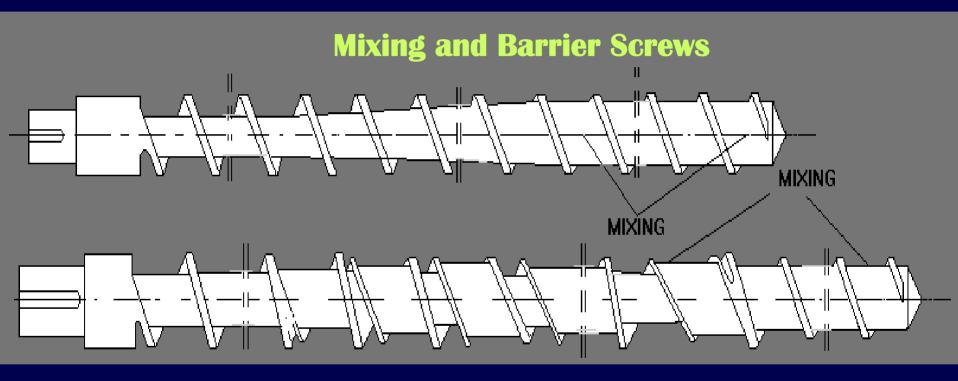
- Melt Film Thickness
- Barrel Temperatures
- Screw Speed



Contiguous Solids Melting

Barrier vs. Single Screw Melting

Single Stage Mixing Screw vs. Barrier Screw



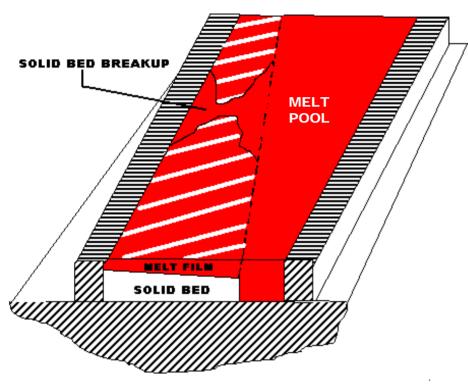
Melting Model – Single Flighted Screw



BARREL

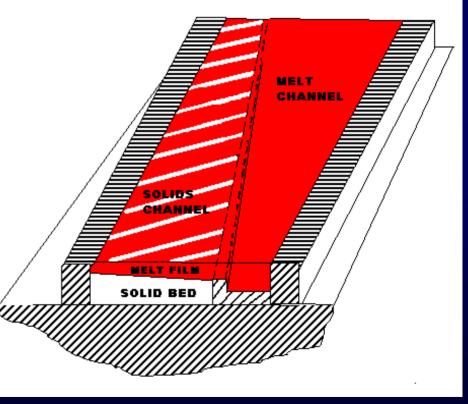
Material Flow

MELTING MECHANISM SEEN IN SCREW PUSH-OUTS



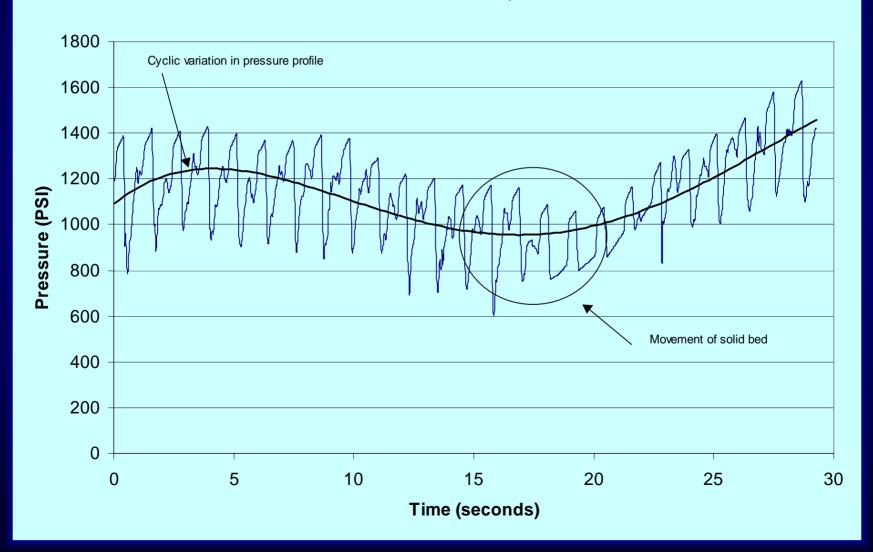
BARRIER SCREW

CONVENTIONAL SCREW

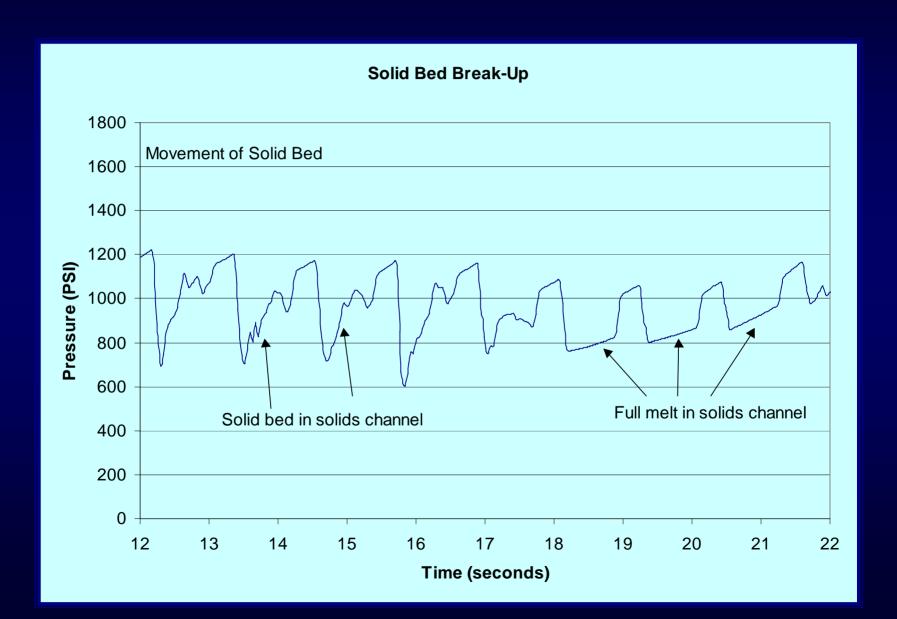


Solid Bed Break-Up

Solid Bed Break-Up



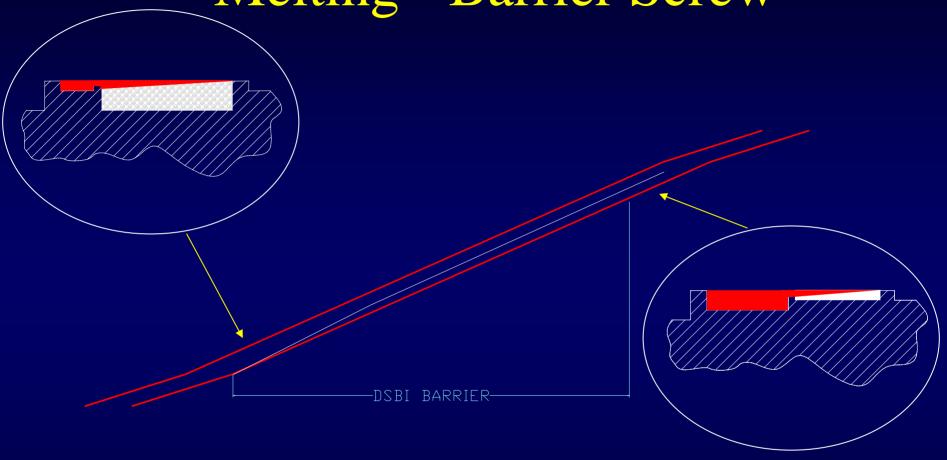
Solid Bed Break-Up

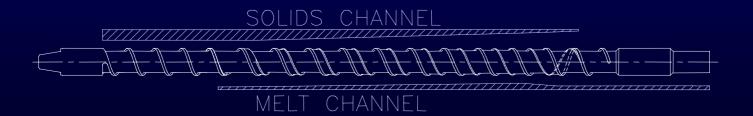


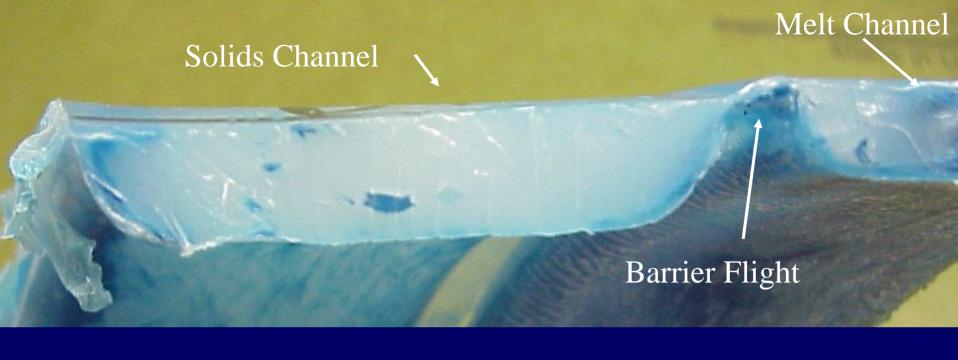
Melting Barrier Screw

- Barrier flight isolates solid bed from melt pool
- Solids and melt channel depths vary independently to accommodate accumulating melt pool and diminishing solid bed
- Critical design variables:
 - Solids channel compression
 - Barrier flight undercut

Melting - Barrier Screw







Mid Barrier Cross-Sectional Photos



Melt Temperature

Influenced primarily by two factors:

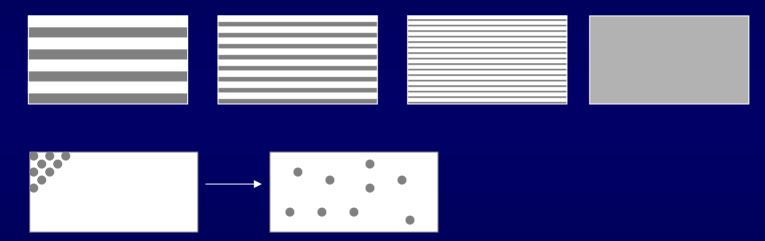
- Conduction
 - = f (residence time, barrel set-points, limitations of heating/cooling units...)
- Viscous Energy Dissipation (VED)
 - = f (viscosity, shear rate...)

Mixing in Single Screw Extrusion

Mixing

DISTRIBUTIVE

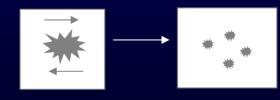
- Increase of interfacial area between two miscible components
- Splitting and recombination of flow streams



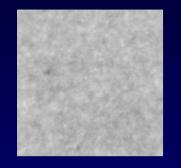
DISPERSIVE

- Shear induced particle size reduction of immiscible components

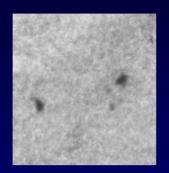




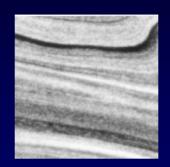
Mixing and Quality



Excellent



Poor Dispersive



Poor Distributive



Poor
Dispersive &
Distributive

- Poor mixing can effect:
 - Physical properties
 - Product Uniformity
 - Aesthetics

Mixing Sections

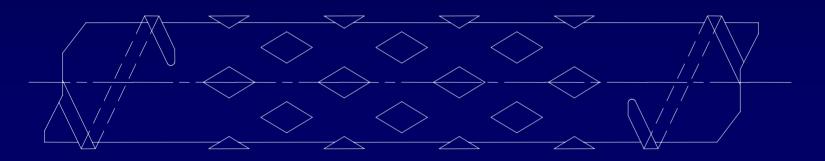
DISTRIBUTIVE

- Pineapple Mixer
- Saxton Mixer
- Dulmage Mixer

DISPERSIVE

- Union Carbide Mixer
- Helical UCC
- Cavity Transfer Mixer

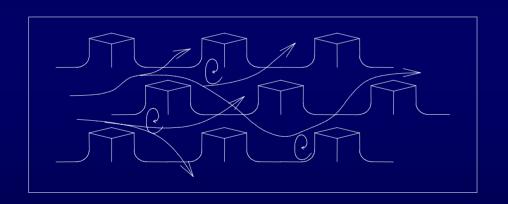
Pineapple Mixing Section

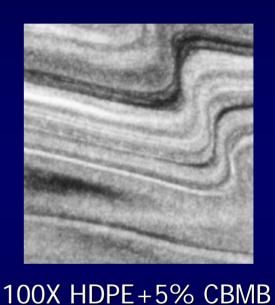




Pineapple Mixing Section

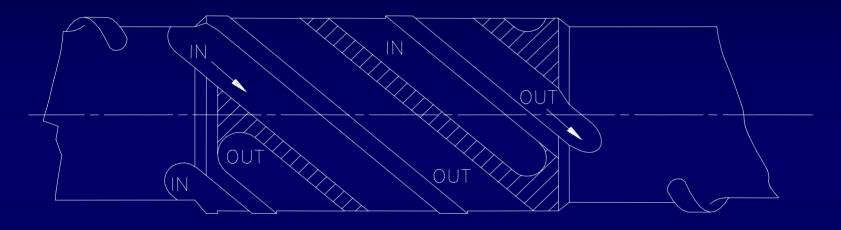






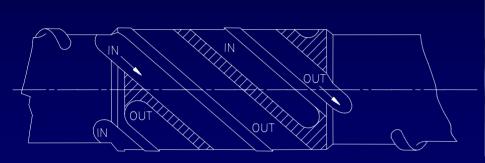
Streamlines Showing Distributive Mixing

Helical Union Carbide Mixing Section (UCC-T)

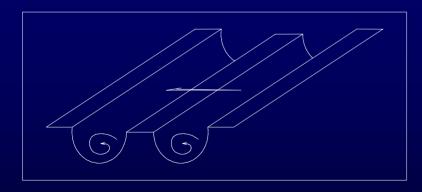




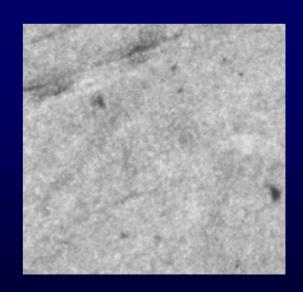
Helical Union Carbide Mixing Flow Pattern







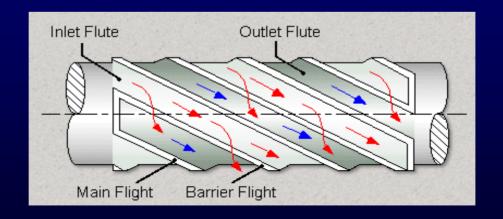
Channel Cross Section



100X HDPE+5%CBMB

EGAN Mixer

- Similar to UCC mixer
- Higher pressure drop
- Intensive shearing
- Surface of barrel not wiped by flight (completely under-cut)



Screw Designs for Extrusion Coating Applications

Conventional Mixing Screws

- Workhorse design for processing extrusion coating resins since the 1960's
- Typical Design
 - 28:1 32:1 L/D
 - Shallow Metering Depth
 - 4:1 Compression Ratio (CR)
 - Single mixing section (Egan or UCC)

Feed Transition Meter Mix Meter

Double Mixing Screw

- A conventional screw with two barrier mixing sections introduced in the 1980's
 - Boost output rate (10-15%)
 - Improve reliability of adhesion at higher outputs
- Higher output applications necessitate the use of a static mixer to improve melt temperature homogeneity across the melt curtain

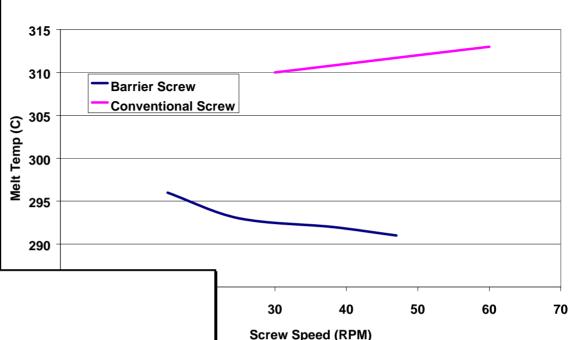
Feed Transition Meter Mix Meter Mix

Barrier Screw Designs

- Recommended for LLDPE and engineering resins in extrusion coating applications
- Also beneficial for lower temperature / higher output polyolefin applications
- Offers superior melting rates and process stability

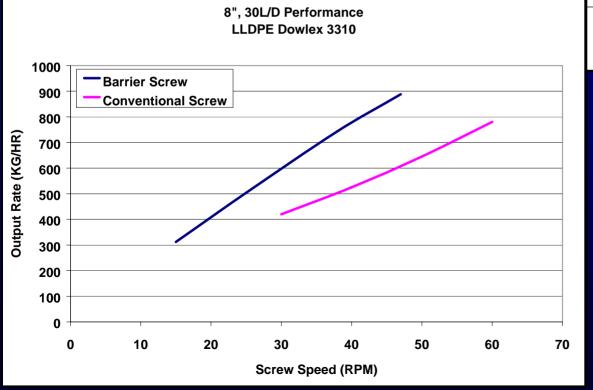
Performance Comparison

8", 30L/D Extruder
Resin: LLDPE Dowlex 3310
Conventional vs. Barrier



8", 30L/D Performance

LLDPE Dowlex 3310



Barrier screw provides higher rate and lower melt temperatures

SCREW COMPARISON

What will I learn?

- Why can't my screw run all resins?
- Why are barrel profiles unique to a screw design?
- Why can increased barrel temperature sometimes result in less output?
- What happens when my screw wears out?

LDPE VS PP COMPARISON

	LDPE	PP
Solid Density (kg/m ³)	920	907
Melt Density (kg/m ³)	750	735
Thermal Conductivity, Solid	0.28	0.22
$(J/s.m.^{\circ}C)$		
Thermal Conductivity, Melt	0.24	0.15
$(J/s.m.^{\circ}C)$		
Heat Capacity, Solid (J/kg.°C)	2300	1700
Heat Capacity, Melt (J/kg.°C)	2300	2100
Melting or Softening Temp, °C	110	163
Freezing or Hardening Temp, °C	90	138
Frictional Coefficient, f	0.3	0.22
Degree of Crystallinity	Low	High
Molecular Weight Distribution	Narrow	Broad

Solid Conveying - PP vs. LDPE

- PP more crystalline, pellets are harder and less elastic. Lower friction between PP and barrel.
- PP has higher melt temperature. Requires longer feed before compression starts.

Melt Conveying - PP vs. LDPE

- Melting rate is limiting factor for PP.
- Melt conveying rate is limiting factor in LDPE

General Screw Design - PP vs. LDPE

- LDPE screw would have shorter feed and faster transition.
- PP screw would have a shallower metering section to help in melting.

Thank You

PRESENTED BY

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