# An Oven Explosion – Lessons Learned on PSM Concepts (or "PSM: It's not just for breakfast anymore")

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# **PSM Concepts & Applicability**

- Should some concepts of PSM be applied in all industries?
- Are codes enough?
- Should we accept the notion that suppliers always know their process and equipment better than us?
- Should we view combustion as something more than a mundane, ubiquitous process?

# The Event

- September 15, 1998: Difficulties starting up new line.
- Once started, operations ramps up to full speed. Ovens ramp up to high fire settings.
- Within 12 minutes of ramp initiation, an explosion, heard for 6 miles, takes place.



# **Evolution or Managed Change?**





# **Sequence of Changes**

- Orders a machine capable of X feet/minute
- Changes order to 1.5 X feet/minute
- Machine manufacturer changes burner requirements
- Burner manufacturer uses same burner, but increases gas flow to get higher rating
- No one changes combustion air fan capability

# **Sequence of Changes**

- Start up problem: Unstable low fire flame
- First Solution: Weighted Pressure Relief Valve on Combustion Air – Too Noisy!
- Second Solution: Combustion Air Trim Damper





Same dP at Two Different Flows Possible 60 -10 0 Trim Damper 3 Affect on Fan Curve 1 n × PRESSURE 6 HP POWER SP 12 2 CAPACITY -1 cfm X 100 16 48 96 32 112 64 80



# The Burner



FM Slabal



### The Incident

- 21:15 Line shut down due to quality; burner at low fire
- 21:34 Line re-started, 12 minute ramp up to maximum speed. Burner demand set to high-fire

21:39 Leakage alarm – calculated number indicating pressure is high within oven. Operators should smell binder fumes. No smell reported. Thermal oxidizer temperature begins rising

### The Incident

21:41 Thermal oxidizer shuts down on high temperature. Machine shutdown initiated, atmospheric bypass opened.
21:41:58 Last of product leaves oven, triggers "sheet break" alarm.
21:45:33 Operator clears alarm
21:46:04 Explosion occurs (pressure disturbance in Zone 1)



# **Explosion Venting**

Recommended by FM & NFPA

 Only for ovens regardless if flammable vapors are generated or not
 Does this mean we do not trust combustion safeguards?

 Venting not provided

# Investigation

- Identified, secured and tested the low combustion air pressure switch
- Confirmed valve positions and determined failure mode – Combustion air trim damper was "fail last"
- Found water in instrumentation lines
- Preserved lines and tested for effect of water on dPT



# **Affect of Water in the Instrumentation Line**

Test No.	Amount of Water	dP Applied (in. WC.)	dP from DPT (in. WC.)	Error (in. WC)
1	0 ml.	4.1	4.1	0
2	5 ml.	4.8	6.0	1.2
3	10 ml.	4.1	5.9	0.8
4	15 ml.	4.12	6.17	2.05
5	20 ml.	4.3	5.1	0.8

Failure to manage change:

 Upsized burner from 30 MM to 40 MM BTU
 Never increased fan rating
 Original specification of 14:1 air/fuel ratio
 Actual ability at high fire was 10:1

• Failure to manage change:

- Due to flame instability at low fire, dP was reduced first by relief valve, then by trim damper
- Fan curve truncated resulting in multipoint dP

 Allowed trim damper to seek low flow position



Failure to properly install:

 Instrument locations changed to become accessible without building ladders/platforms
 Tap points were higher than instruments
 Condensate filled lines
 Induced error
 Corroded switch contact closed

Questionable design of burner

 Seemed to meet code, but high fire flame was not monitored
 Low fire flame monitored and stayed lit
 Became ignition source of explosion

- We are not measuring meaningful parameter
  - Combustion air pressure limits do not mean we have sufficient air for combustion!
- We assume linkage will not slip or bind
  - Linkage slip has happened!

- Should we measure air and fuel flow instead?
   – Ratio control and interlock systems?
- How about measuring combustibles in the exhaust?
- Can we make them reliable enough to preclude the need for venting?
   – ASME Code Case 2211?
   – SIL 1 or 2 needed?