# BASIC INDUSTRIAL DRYING

# **TAPPI**

#### Building and Industrial Mat 2011 Spring Meeting MAY 18 – 20



Excellence in Process Heating™

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## **SESSION AGENDA**

- 1. DEFINING THE PROCESS REQUIREMENTS
- 2. "CONVENTIONAL" DRYING METHODS
- 3. UNDERSTANDING THE DRYING/HEATING PROCESS
- 4. UNDERSTANDING CONVECTION DRYING
- 5. UNDERSTANDING INFRARED DRYING
- 6. EQUIPMENT SELECTION: PROS AND CONS

#### DEFINING THE PROCESS REQUIREMENTS

- **Drying**; Solvent vaporization/evaporation
- **Curing**; A final web/coating temperature requirement (normally following a drying requirement)
- **Heating**; Raising the temperature of a product: Substrate Heat set? Curing? Before lamination?; film, foils, etc.

<u>CONVENTIONAL TECHNOLOGIES USED FOR</u> <u>DRYING, CURING AND HEATING A WEB</u>

#### CONVECTION SYSTEMS

- IMPINGEMENT DRYING
- FLOATATION DRYING
- THROUGH AIR DRYING
- BATCH DRYERS/OVENS

#### RADIANT HEATING/DRYING SYSTEMS

- ELECTRIC INFRARED

- GAS FIRED INFRARED



Heating a Web







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#### **DEFINING CONVECTION:**

- "The transfer of heat by circulation of a gas or a liquid in contact with the object to be heated."
- Convection dryers use 'conditioned' (Temperature and humidity controlled) hot air for heat transfer.
- Liquid Vaporization and Evaporation by both heat conduction and turbulent air flow.
- Convection dryers use a Nozzle array or ducted distribution of the air to uniformly heat the product as it passes through the confined Dryer atmosphere

#### CONVECTION DRYER HEAT LOADS – 100% FRESH AIR DESIGN











# Factors that impact Heat Transfer

#### by Impingement:

- Velocity effect on Heat transfer is approximately proportional to the 0.6 power of the change. (V<sup>1</sup>/V<sup>2</sup>)<sup>0.6</sup>
- **Drying air temperature** increase or decrease will yield an approximate linear change in heat transfer.
- Humidity of the Supply air (Low Exhaust/High Recirculation) will reduce the heat transfer. This is due to a lowering of the dT used when a higher wet bulb temperature (higher moisture content in the Exhaust/Return air) vs. the dryer supply temperature is present.
- Nozzle Distance from the web impacts the 'Effective' heat transfer (seen on the web surface) by approximately 10% per inch of distance; *i.e.:* A 1 inch nozzle to web distance will achieve 20% more theoretical heat transfer than a nozzle 3 inches away.



Theoretical Impingement Heat Transfer vs. Temperature/Velocity

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- ✓ Heat transfer input (Velocity/Temperature) is somewhat independent of web handling issues.
- Can be easily arranged for multiple heat transfer zones, and also easily changed for different products requirements
- ✓ Accurate and uniform control of the dryer temperature for heating products irregardless of shape, size or color.
- Multiple Nozzle configurations and web pass configurations can be used with heat transfer to the top and/or bottom side of the web as required.
- Cost effective and can be adapted to multiple products with simple velocity and temperature adjustments.

#### **IMPINGEMENT NEGATIVES**

- Roll or conveyor support needed along with the associated initial costs, maintenance issues, and web tension requirements for longer dryers.
- Possibility of Web Scratching or marking from contact with web support idlers.
- Lower rates of heat transfer and heating by conduction from the surface being impinged on (Thicker products will take longer to heat).
- Limitation of heat transfer velocities which may disturb or contaminate the coating.
- Generally slow to heat up to operating levels and slow to cool down which results in the limitation of maximum operating temperatures that may be dictated by the web properties.

# **FLOATATION DRYERS**











Controllable Sine Wave Web path

# <u>FLOATATION NOZZLE</u> <u>ARRAY</u>



#### **FLOATATION DRYER ADVANTAGES**

- ✓ Non-contact web support eliminating issues with marking or scratching.
- ✓ Eliminates the need for support rolls or conveyor with obvious benefits for running a saturated or 2-side coated web.
- ✓ Sine wave float eliminates edge curl.
- ✓ Positive web tracking through the dryer ('self centering') with minimum tension requirements.
- Accurate and uniform control of the dryer temperatures.
- Nozzle input from both sides of a coated web increases heat transfer capability and shortens the dryer length needed in most cases as compared to one side impingement.

#### **FLOATATION NEGATIVES**

- Lower rates of heat transfer and heating by conduction from the surface being impinged on (Thicker products will take longer to heat).
- Boundary layer breakup is better with impingement, but, the Coanda creates parallel flow averaging of heat transfer.
- ✓ Limitation of heat transfer velocities which may disturb or contaminate the coating.
- ✓ Velocity and flow balance needed to float against line tension may limit heat transfer.
- ✓ Generally slow to heat up to operating levels and slow to cool down which results in the limitation of maximum operating temperatures.

# <u>THROUGH AIR DRYING</u> <u>SYSTEMS</u>



# Supply Air



#### FLAT BED THRU AIR DRYER

HIGH TO MEDIUM PERMEABILITY (dP UP TO 6" W.C.)





MEDIUM TO LOW PERMEABILITY ( dP CAN BE OVER 20" W.C.)

#### THROUGH AIR ADVANTAGES

- ✓ 2 to 3 times higher Air flow (Heat Transfer) than conventional convection.
- Intimate contact with product interior heats uniformly and rapidly.
- High thermal efficiency for Heating, cooling or Drying applications.
- Accurate and uniform temperature control to heat "through" the product.
- Extremely high evaporation rates from a combination of mechanical and thermal drying.
- $\checkmark$  Enhances the 'Hand' of Non woven materials.
- Self tracking suction beds and Simple operation.

#### THROUGH AIR NEGATIVES

- $\checkmark$  Dependent on Permeability of the web.
- ✓ Wet to dry permeability changes in the web properties require multiple zones for Fan selection and efficient operation.
- ✓ Higher Blower Pressure drop needed for the higher air flow rates and to overcome product pressure drops; requires higher HP than convection in most cases.
- ✓ Mechanical losses of fiber and coating are carried in the through air stream.
- ✓ Most Products require a support conveyor or screen to maintain the 'Flat' bed with associated maintenance costs.



"The transfer of heat via electromagnetic waves between the heat source and the object to be heated."

#### **Electromagnetic Energy Spectrum**



#### **INDUSTRIAL PROCESS INFRARED**

- Wavelengths used for Industrial Infrared heating applications range from 1.17 micron (4000° F) to 5.4 micron (500° F).
  - Short Wave Emitters 2150° F to 4000° F
  - Medium Wave Emitters 900° F to 2150° F
  - Long Wave Emitters 500° F to 900° F
- Wavelength is inversely proportional to the temperature of the emitter. (i.e.: As temperature increases; the wavelength decreases)

#### **Infrared Spectrum**



### Efficiency of Industrial Infrared Emissions



# Stefan Boltzman Law to Determine

#### **Infrared Power**

The total energy radiated is equal to the

black body temperature to the 4<sup>th</sup> power

# $\mathbf{Q} = \mathbf{k}\mathbf{T}^4$

- Q = Emitted Energy
- k = Constant (0.172 x 10<sup>-8</sup>)
- T = Source temperature (°K)

*For example:* If the temperature of the emitter is increased by 50%, the energy emitted is increased by 500%

# **Determining Wavelength**



#### Wien's Law

The peak wave length of emission of an infrared heater can be calculated by Wien's Law

 $\lambda = C/T$ 

- $\lambda$  wavelength in microns
- C Constant (2898)
- T Source temperature (°K)

## **Typical IR Absorption Curves**



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#### **Infrared Advantages**

- Higher rate of heat transfer/Square Ft. compared to Convection
- Floor space savings due to higher density Heat output
- Easy to zone for uniform heating of the product and range of widths being processed.
- ✓ Fast response to changing process conditions
- Quick start up and shut down in most styles of heaters
- ✓ 'Infinite' temperature control and 'tune-ability' with Electric IR Source.
- ✓ Lower initial capital and installation cost
- Easily added to existing conventional dryers to increase line speed
- ✓ Infrared/Air dryers suitable for solvent based coatings

#### **Infrared Negatives**

- Some coatings may not be able to take advantage of higher rates of heat transfer and may skin and blister
- Difficult to work with temperature sensitive substrates
- Electric Source Infrared Kw costs are generally higher than equivalent gas costs – (direct energy cost comparisons)
- Gas Fired IR has limited turn down and control. Sizing is job specific.
- Since IR is basically a surface conduction phenomenon, harder to dry heavier coatings rapidly without overheating the surface
- ✓ Almost essential to run trials in lab or on a pilot line to confirm dryer sizing and desired finish product.

# To Sum it All up .....



# Which Drying Method is the Best for the Application ??

# Convection ?Infrared ?Other ?

# <u>ANSWER:</u> <u>NO SINGLE METHOD</u>

- Product and Web handling issues should always be considered a part of the decision.
- Best Design and Efficiency will normally be a combination of the available technologies.
- ✓ Use and consider the advantages (and Negatives) of each.
- Input the features needed to handle special product requirements, cleaning, maintenance, and ease of operation.







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