

Black Liquor Evaporation

Optimizing Performance

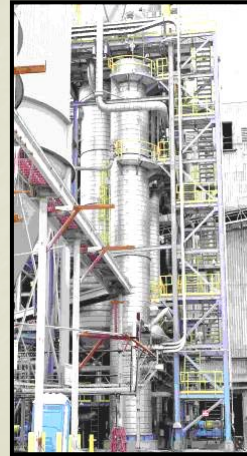
Jean-Claude Patel
A.H. Lundberg Associates, Inc.
Naperville, IL

Topics

- Introduction
- Surface Condensers & Vacuum Systems
- Condensate Segregation
- Mist Elimination
- Hybrid Falling Film / Rising Film Trains
- FC Concentrator Upgrades

A New Era for the P&P Industry

- Environmental regulations
 - Tightening of the liquor cycle
 - Reduced color and BOD discharges
 - Foul condensate stripping
 - Higher NPE load in recovery island
 - Higher firing liquor %TS
 - NCG Collection
 - Reduced air emissions.



A New Era : Environmental Regulations

- Energy Cost
 - Financial viability of operations
 - Reduce energy usage
 - Optimize on-site energy production processes
 - Get more efficient = Be more competitive

A New Era for the P&P Industry

- Evaporation plant
 - Biggest consumer of steam & cooling water
 - Emphasis: Better performance & energy efficiency
 - Modernize and upgrade evaporation facilities.



Typical Upgrade Programs

- Gain BL throughput and concentration
 - Often well above original design
 - Retire older less efficient evaporator trains
- Condensate segregation
 - Reduced foul condensate generation
 - Minimized stripping or biological post-treatment costs
 - Improved condensate re-use within the mill

Typical Upgrade Programs

- Reduce liquor entrainment
 - Minimized soda losses
 - Re-use of process condensate
- Look at the whole recovery island
 - WBL composition & %TS (Recaustizing/Washers)
 - Evaporators= Source/Sink for low grade heat
 - Concentrator upgrades for higher solids
 - Indirect Liquor Heaters

Typical Upgrade Programs

- Optimize each design parameter individually
 - Unique features of the evaporators
 - Where are the weak links?
 - Liquor properties
 - Can they be improved? (Whole mill issue)
 - NPE Removal
- Overall Power & Recovery configurations
- Upgrade goals & Budget limitations

Typical Upgrade Programs

- Review a few examples
 - Common performance problems with the MEEs
 - Typical upgrade programs that can be undertaken.
- *Caution*
 - *What worked well at some location may not be appropriate at another.*

Surface Condensers & Vacuum Systems

- Insufficient vacuum
 - Most common operating problem encountered
 - Poor vacuum lowers available working ΔT
 - Translates into a loss in evaporation capacity



Poor Vacuum Impact on ΔT

- Steam Temperature: 274 °F
- Condenser Temperature: 132 °F
- Actual ΔT : 98.3 °F inclusive of losses due to BPR

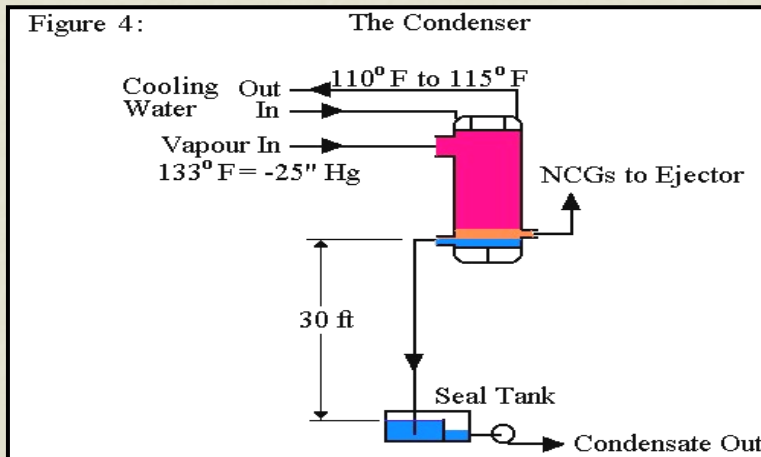
Vacuum	Cond. Temp.	Actual ΔT	Gain/Loss
25.5 "Hg	129.0 °F	101.3 °F	+3.0%
25.0 "Hg	132.0 °F	98.3 °F	-
24.0 "Hg	140.0 °F	90.3 °F	-8.1%
23.0 "Hg	146.5 °F	83.8 °F	-14.7%
22.0 "Hg	152.0 °F	78.3 °F	-20.3%
21.0 "Hg	156.7 °F	73.6 °F	-25.1%
20.0 "Hg	161.0 °F	69.3 °F	-29.5%

Surface Condensers & Vacuum Systems

- Need higher steam pressure
 - Actual ΔT raised back up
 - Capacity re-gained
 - Steam economy is lost due to additional preheat loads



Surface Condensers & Vacuum Systems



Vacuum Systems

- Many vacuum systems are grossly undersized
 - Evaporator capacity has been pushed without consideration for achievable vacuum
- Poor NCG pre-cooling is also very common
 - Higher volume to evacuate due to moisture
- Excessive air leakage
 - Maintenance issue
- Surface condenser problems

Surface Condensers

- Insufficient condensing surface
 - Unrealistically high heat transfer coefficient was used
- Solutions:
 - Install an auxiliary condenser
 - Increase water flow
 - Run at higher condensing temperature thus higher steam pressure (costly)

Surface Condensers

- Insufficient water flow
 - Excessive usage elsewhere
 - Worn water pump
 - Inadequate piping, flow restrictions
 - Fouled tubes on the water side
 - CaCO_3 scale from hard water, etc.
 - Biological slime
 - Hydroblasting of the tubes required



Surface Condensers

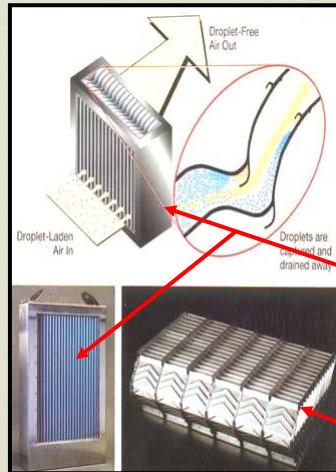
- Leaky water boxes
 - Water short-circuits one or more passes
 - Some condensing area effectively by-passed
- Inadequate NCG venting
 - Typically due to poor shell baffling set-up
 - Pockets of gas accumulate in some areas of the shell
 - Additional vent nozzles may have to be installed

Surface Condensers

- Shell side fouling
 - Excessive, even if infrequent, entrainment or foaming
 - Dried up liquor
 - Anthraquinone
 - Removal is difficult
 - Best accomplished by boiling with specialty chemicals
 - Upgrade mist eliminators



Mist Elimination

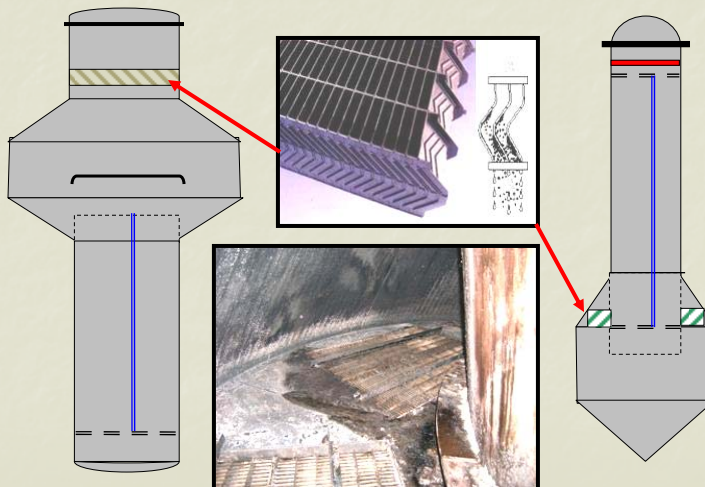


- Minimize black liquor carry-over in vapors sent to the next effect.
- Occurs in all the bodies but most prominent in vacuum effects.

Horizontal Flow

Vertical Flow

Mist Elimination



Mist Elimination

- Impact on operation of excessive entrainment
 - Chemical (soda) loss
 - Compensated via additional salt-cake make-up (Cost)
 - Fouling of heating elements and condenser
 - Translates into poor heat transfer, higher ΔT
 - Color contamination in condensate
 - May prevent re-use within the pulp mill
 - Poor stripping efficiency
 - Fouling of stripper preheaters
 - Foaming in stripper column

Mist Elimination

- Possible causes for excessive entrainment
 - Pushed evaporation capacity
 - Not enough elimination capacity
 - Fouled, damaged or dislodged mist eliminators
- Retrofit to horizontal flow mist eliminators
 - Accommodate high vapor loadings
 - High removal efficiency: $\sim 5\text{-}20$ ppm Na_2O

Mist Eliminator Retrofit in LTV

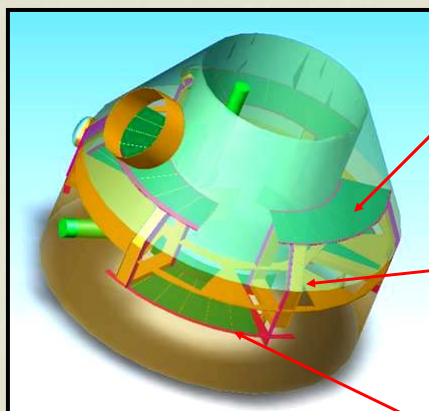


Old centrifugal type



New chevron type

Mist Eliminator Retrofit in FF

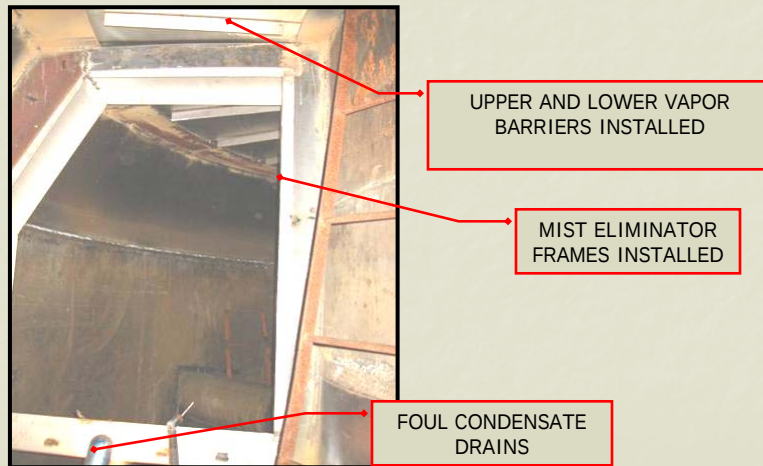


UPPER VAPOR BARRIERS
(3 SECTIONS)

VANE BANK
FRAMES
(6 MODULES)

LOWER VAPOR
BARRIERS (3 SECTIONS)

Mist Eliminator Retrofit



Mist Eliminator Retrofit



Condensate Segregation

- Water reduction = Energy reduction = Cost savings
 - Annual cost for a typical bleached mill

\$ 1.0 – 3.0 MM/year

- MEEs are the major “water-treatment” plant to produce condensate suitable for re-use

Condensate Segregation

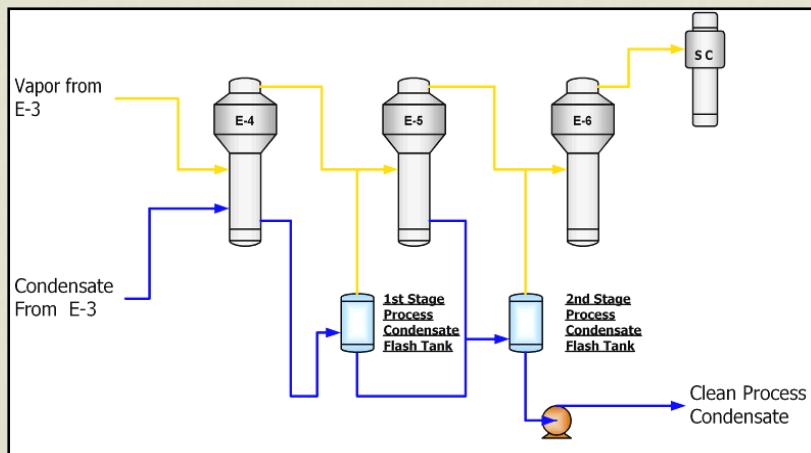
- Volatile components (Methanol & TRS)
 - Quickly stripped from the WBL in the first two stages of evaporation (typ. 5th & 6th effects)
 - Highest contamination found in condensate resulting from 5th and 6th effect vapors
 - ~ 75% of the volatile BOD
 - Most of the TRS compounds
- Keep cleaner condensate from MEEs front end away from this contaminated condensate

Condensate Segregation – Step One

- Remove 4th effect condensate and flash in external FT
 - Maintains overall economy
 - Flashing further removes volatile contaminants
- Methanol under 150 ppm (typ.), TRS at a few ppm
 - Suitable for re-use on the brownstock washers



Condensate Segregation – Step One



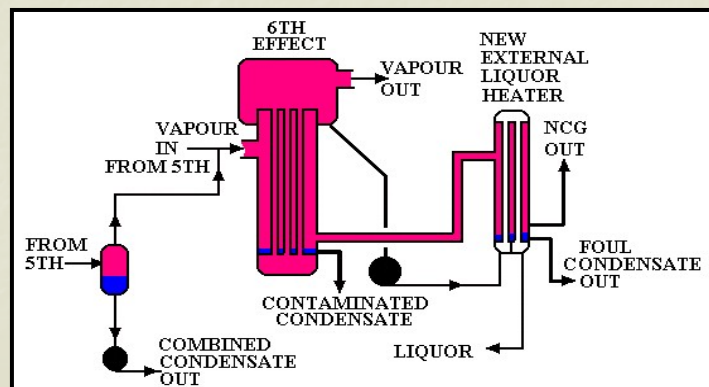
Condensate Segregation – Step Two

■ Principle

- Contaminants being more volatile than water tend to condense later than water vapors
 - Condensing contaminated vapors in two stages – in series – effectively moves most of the contaminants into the second condensing stage
- Fairly clean condensate produced out of the 1st stage
- Very foul condensate collected from the 2nd stage

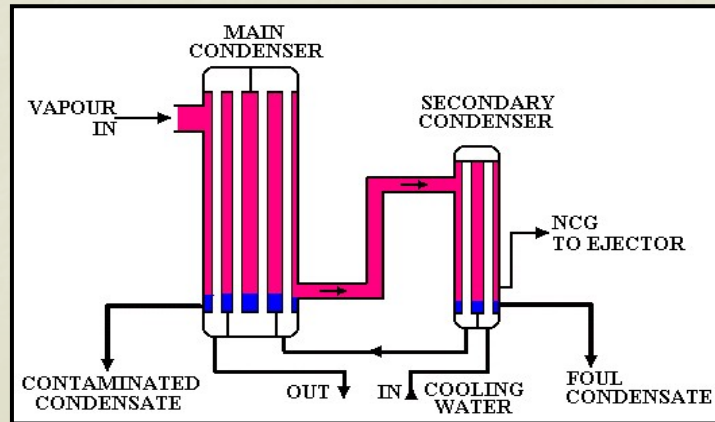
Condensate Segregation – Step Two

- Modify older LTVs by adding external heaters



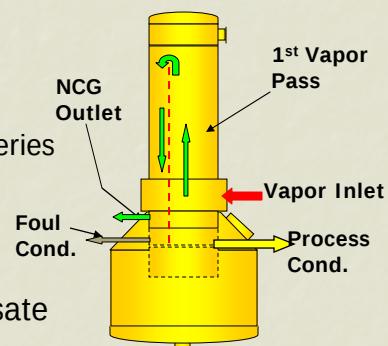
Condensate Segregation – Step Two

- Modify existing condensers the same way



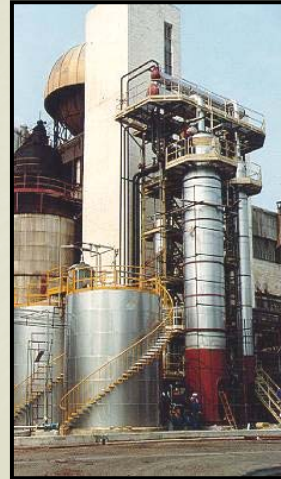
Condensate Segregation – Step Two

- Modern FF & Condensers
 - Two-stage condensing built-in
 - Baffling of the shell
 - Two condensing sections in series
- Slightly contaminated condensate collected in the 1st vapor pass
- Foul condensate in the 2nd pass



Condensate Segregation – Step Two

- Contaminated condensate
 - Methanol level typically ~ 400 ppm
 - Suitable for re-use in recausticizing
- Foul condensate
 - Methanol level often > 6,000 ppm
 - Requires stripping before re-use



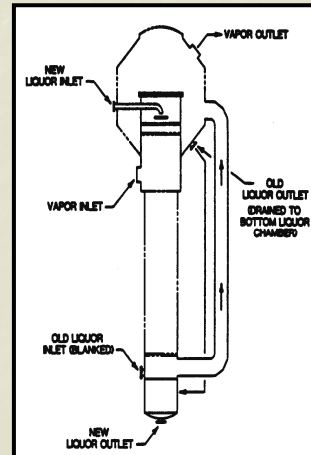
Hybrid Systems FF / LTV

- FF unit integrated with LTVs
 - Used to gain capacity
 - FF designed for lower Delta-T
 - Some driving force is freed
 - Used to push other effects harder
 - Overall capacity gain for the set
- *Other factors (SC, entrainment, etc.) may limit the actual capacity gained*



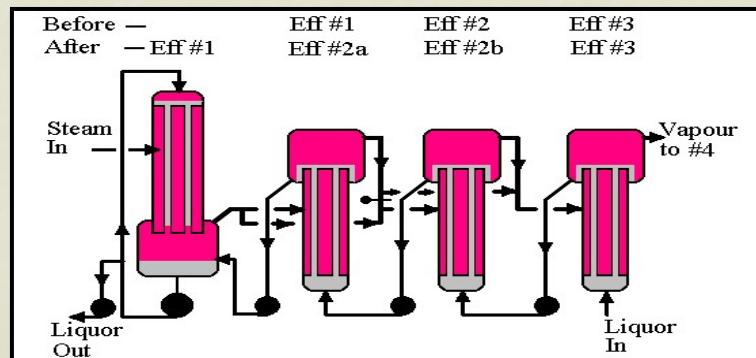
Hybrid Systems FF / LTV

- LTV Conversion to FF
 - Bottom liquor box extension
 - New distribution device
 - New recirculation pump & piping
 - New vapor piping
- Typically done to reduce steam pressure needed at the front end



Hybrid Systems FF / LTV

- New FF as first effect provides better resistance to scale and greater turndown



Hybrid Systems FF / LTV

- Conversion from 5 to 6 effect operation
 - New FF body added to LTVs
 - Evaporation capacity gained: ~ 17%
 - Load on existing effects: ~ same
 - No additional steam or cooling water
 - Many conversion projects driven solely by energy savings, not capacity gained

Hybrid Systems FF / LTV



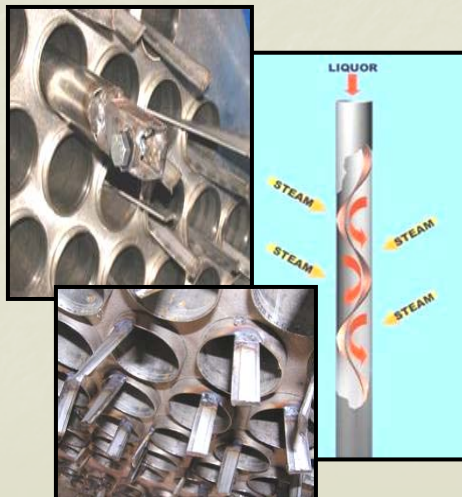
- FF body as 1st or 6th effect?
 - Heat transfer characteristics of the train
 - Where is the weak link?
 - Concentration profile changes across the train
 - Check materials
 - FF easily foam at low solids
 - LTV foul at higher solids

FC Concentrator Upgrade

- Utilities can help finance power savings projects
 - Quick, easy and reliable source of savings
- Ideal candidates
 - Existing FC concentrators and heavy liquor heaters
 - Retrofit with turbulence enhancers



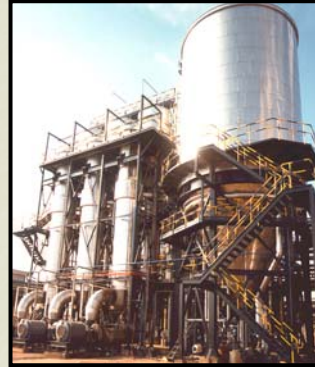
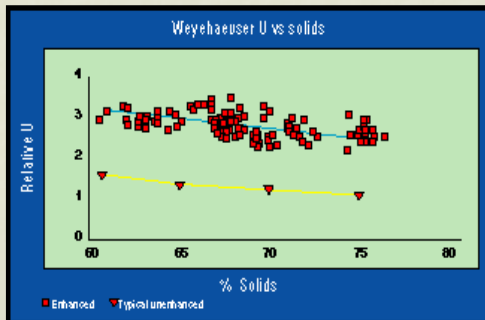
Reynolds Enhanced Crystallizer (REX)



- Spiral inserts disrupt boundary layer at the tube wall
- Apparent Re in the turbulent region even at high liquor viscosities
- More efficient use of HP
 - High U coefficient
 - Lower tube velocities

Net Benefits of REX Upgrades

- Recirculation rate cut in half
- U Coefficient doubled
- Lower tube-side Delta-P
- 45-50% power savings



Conclusions

- MEEs total energy usage
 - Varies greatly from mill to mill
 - Age of the facility & capital invested over the years
 - Integration of ancillary equipment (stripping, etc.)
 - Type of evaporator (LTV, FF, etc.)
 - Environmental limits
- Different justifications at each mill



Conclusions

- Benchmarking
 - Critical to assess performance of your MEEs for energy consumption & costs against others
 - Identify MEE performance & energy use inefficiencies
 - Upgrade program developed & justification established
- Implementing such program
 - Significant improvement to the bottom line

\$\$\$\$